

BLOW MOLDING (4.8 gpm/ton at 65 psi) HDPE = 40 #/hr/tonPET = 40 #/hr/tonLDPE = 45 #/hr/tonPP = 45 #/hr/ton**BLOWN FILM** Nominal Air Flow CFM Single Lip Air Ring = 75 CFM/inch Dual Lip Air Ring = 150 CFM/inch Cooling Ton/1000 CFM Nominal Tons Air Temp to Air Ring **Air Inlet Conditions** 40°F 50°F 95°F drv bulb/65°F wet bulb 17.9 tons 11.3 tons 100°F drv bulb/80°F wet bulb 189 tons 12.1 tons 65°F dry bulb/56°F wet bulb 6.8 tons 2.9 tons Internal bubble cooling - $(\text{gpm x }\Delta T)/24 = \text{chiller ton}$ Q (BTUH) = 4.5 x CFM x ΔH EXTRUSION Coating (12 gpm/ton for direct roll cooling) LDPE = 40#/hr/ton Pipe & Profile (Minimum 4.8 gpm/ton) ABS = 80 #/hr/tonHDPE = 50#/hr/ton PVC = 90#/hr/ton Sheet (8 gpm for direct roll cooling) ABS = 75#/hr/ton LDPE = 55#/hr/ton PS = 75#/hr/ton HDPE = 50#/hr/ton PP = 55 #/hr/tonPVC = 80#/hr/ton UHMWPE = 40#/hr/ton Machine Cooling (85°F)

Feed throat cooling = 0.33 ton/inch Gear box cooling = 0.5 ton/inch

Screw cooling = 0.5 ton/inch Barrel cooling = 1 ton/inch

THERMOFORMING

 Minimum process flow of 4.8 gpm/ton

 HIPS = 250#/hr/ton
 PVC = 240#/hr/ton

 PE = 180#/hr/ton
 Rail Cooling = 3 tons

 Mold Cooling - Tempered water required 80°F-110°F

WEIGHED WATER TESTS

Chiller = 2.4 gpm/ton @ 50°F LWT (@ 10°F Δ T)(Nominal Design) Cooling Tower = 3 gpm/ton @ 85°F LWT (@ 10°F Δ T)(Nominal Design)

 $(\text{gpm x }\Delta T)/24 = \text{chiller ton}$ (#/min x ΔT)/200 $(\text{gpm x }\Delta T)/30 = \text{tower ton}$ (#/min x ΔT)/250

1 Refrigeration Ton = 12,000 BTUH 1 Cooling Tower Ton = 15,000 BTUH

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INJECTION MOLDING

PC = 50 #/hr/ton

PP = 35 #/hr/ton

PET = 40#/hr/ton

Nvlon = 40#/hr/ton

Mold Cooling

ABS = 50 #/hr/tonAcrylic = 35#/hr/tonHDPE = 30 #/hr/tonLDPE = 35 #/hr/ton

Machine Cooling

10 hp hydraulic motor hp = 1 ton Feed throat cooling = 1 ton (machines under 500 ton use $\frac{1}{2}$ ton) Hot runner molds = 1 ton/10.5 kW hot runner

COMMON VALUES

Mold room heating = 25 BTUH/ft² Mold room cooling = 80 BTUH/ft² Non-mold room heating = 50 BTUH/ft² Water pump = 0.1 ton/hp Chiller capacity loss = $20\%/10^{\circ}F$ BTUH = $\operatorname{gpm} x 500 \times \Delta T$ (water) Air comp., w/o after cooler = 0.10 ton/hp Air comp., w/ after cooler = 0.20 ton/hp

Hydraulic = 0.1 ton/hpVacuum pump = 0.1 ton/hp $Q = M' x C p' x \Delta T$

PPO = 40 #/hr/ton

PS = 50 #/hr/ton

PU = 40 #/hr/ton

PVC = 65 #/hr/ton

% Polypropylene Glycol (Volume vs Freeze Protection) $20\% = 20^{\circ}F$ $30\% = 10^{\circ}F$ 40% = -5°F $50\% = -25^{\circ}F$

PIPE SIZING GUIDE (Based on 10' hd loss/100' pipe)

1⁄2″ = 2 gpm ³/₄" = 5 gpm 1'' = 10 gpm1¼″ = 20 gpm 11/2" = 30 gpm

A A A A

2'' = 50 gpm $2^{1/2''} = 90$ gpm 3" = 160 gpm 4" = 320 gpm 5" = 525 gpm

6" = 900 gpm 8" = 1,800 gpm 10'' = 2.500 apm12" = 3,300 gpm

CHILLER FLOW RATES VS TEMP DIFFERENCE PER TON

1.2 gpm = 20°F ΔT 2.4 gpm = $10^{\circ}F \Delta T$ (Nominal Design) $4.8 \text{ gpm} = 5^{\circ}\text{F} \Delta \text{T}$ 9.6 gpm = $2.5^{\circ}F \Delta T$

COMMONLY USED EQUIVALENT & EQUATIONS

Pump BHP = (apm x ΔP (Ft Hd)/(3.960 x Pump Eff) Heat Exchanger = Q = U-factor x area x ΔT kW = (amps x volts x 0.85 x 1.73)/1.000 1 kW = 3.413 BTUH $1 \, \text{kW} = 1.34 \, \text{hp}$ PSI = ft of head/2.31(°F - 32) x 5/9 = °C

1 HP = 2,544 BTUH 1 gallon = 8.33 lbs (water) $1 \, \text{ft}^3 = 7.48 \, \text{gal} \, (\text{water})$ PSI = 14.5 bar $(^{\circ}C - 9/5) + 32 = ^{\circ}F$

TOWER WATER MAKE-UP

Untreated = 2% of Flow Rate

Treated = 1.5% of Flow Rate

CONSULT FACTORY FOR OTHER CONDITIONS

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